

Factsheet

26 feb. 2009

Cryogenic cooling

Cryogenic cooling uses phase change for cooling: sublimation of dry ice (solid CO₂) or evaporation of liquid CO₂ or N₂. The solid or fluid is produced in large-scale centralised plants, mostly as by-product of a chemical process (for instance ammonia production). The cold can be applied in de-central applications, including mobile applications. Especially the use of dry ice is technically quite simple, because no electrical driven cooling equipment is needed. Dependent on the situation safety measures may be needed.

Although CO₂ is considered a by-product of industrial processes, cryogenic CO₂ is not available for free. Usually it comes available from regenerating gas washing fluids; the CO₂ will be available in (concentrated) gas form. This gas can be cooled and compressed for production of fluid CO₂. For production of solid CO₂ (dry ice), the fluid is adiabatically expanded (resulting in evaporation of about half of the CO₂ and solidification of the remainder). Fluid N₂ is produced by compressing air.

Practical benefits

- silent (most relevant for mobile applications);
- very suitable for "refrigerated delivery": by adding some dry ice to a delivery, cooling is ensured for a certain period without need of power supply;
- high quality cold: low temperatures (far below the freezing point);
- buffer is very suitable for "peak shaving".

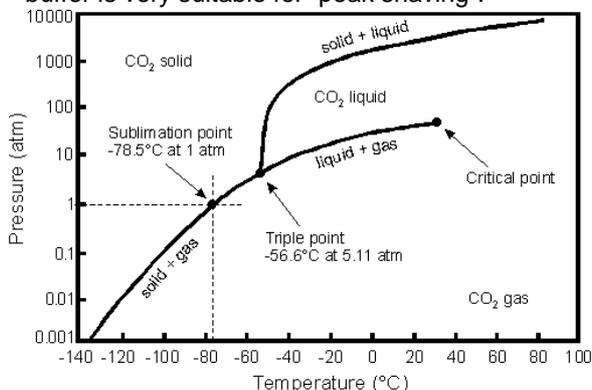


Figure 1. Pressure-Temperature phase diagram for CO₂.

Energetic considerations

Solid CO₂ at atmospheric pressure (sublimation point -78.5°C) has a latent evaporation heat of 571kJ/kg, whereas the specific heat (C_p) of CO₂ gas is 0.85kJ/(kg K). Thus, for cooling applications the evaporation of solid CO₂ will remove about 640kJ per kg CO₂. When producing cryogen CO₂ a comparable amount of heat is removed from the gas, combined with compression; the exact amount of energy needed depends on the efficiency of the process. Since this is

low-temperature cooling, generally this is less efficient than refrigeration cooling. Furthermore, it should be taken in account that losses in the supply chain will occur.

For cooling far below the freezing point, however, COP of mechanical cooling is low too; energetic performance of cryogenic cooling and mechanical cooling will be more comparable.

Energetic efficiency of using cryogenic (fluid) N₂ is slightly lower than for CO₂ because fluid N₂ is produced from air (which has other components that hinder the process efficiency) whereas fluid CO₂ is produced from nearly pure CO₂ gasses. However, fluid N₂ has some practical advantages: it can be kept fluid at atmospheric pressure.

Financial considerations

Costs of investments largely depend on the specific situation; no general indicative figures can be given. Indicative prices of cyrogen CO₂ and costs of cooling:

- Fluid CO₂ (bulk amounts) €0.06 to €0.10 per kg (price 2006); cooling potential about 300 to 400 kJ/kg (dependent on temperature and pressure). Resulting variable costs for cooling €0.15 to €0.33 per MJ.
 - Dry ice (small amounts): about €1 per kg; cooling potential 640 kJ/kg. Cooling costs about €1.60 per MJ.
- For reference: energy costs for mechanical cooling are about €0.008 per MJ (with E-tariff €0.10/kWh and COP 3.5).

Conclusions

Generally, cryogenic cooling is energetically less efficient than mechanical cooling. Financial feasibility will depend on the specific situation.

Sources and further info

www.airliquide.com

Feron PHM and CA Hendriks (2005): CO₂ Capture Process Principles and Costs. *Oil & Gas Science and Technology* Vol. 60 (2005), No. 3.

Contact: Jan Broeze, AFSG Wageningen UR, phone +31.317.480147, e-mail jan.broeze@wur.nl
Sietze van der Sluis, TNO, Phone +31.88.8662206 email Sietze.vanderSluis@tno.nl

This renewable cooling research is executed with practical input by NVKL and financial support by the Dutch Ministry of Economic Affairs; program *Energie Onderzoek Subsidie: lange termijn (EOS-LT)*.